

Fig. 1 : Effect of the support for the catalytic elimination of N_2O
VVH = 35000 h^{-1} ; 3% O_2 , 2000 ppp N_2O , 2000 ppm NH_3 , temperature increasing
($5^\circ\text{C}/\text{min}$)

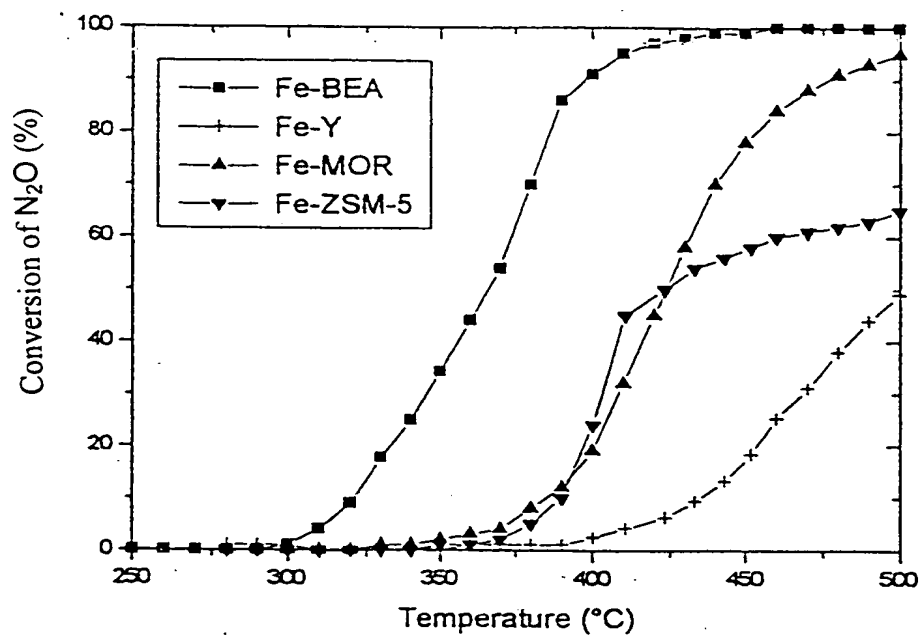


Fig. 2a : Influence of the presence of NH_3 on the catalytic elimination of N_2O in the presence of 3% O_2 , $\text{VVH} = 35000 \text{ h}^{-1}$, 3% O_2 , 2000 ppm N_2O , He.

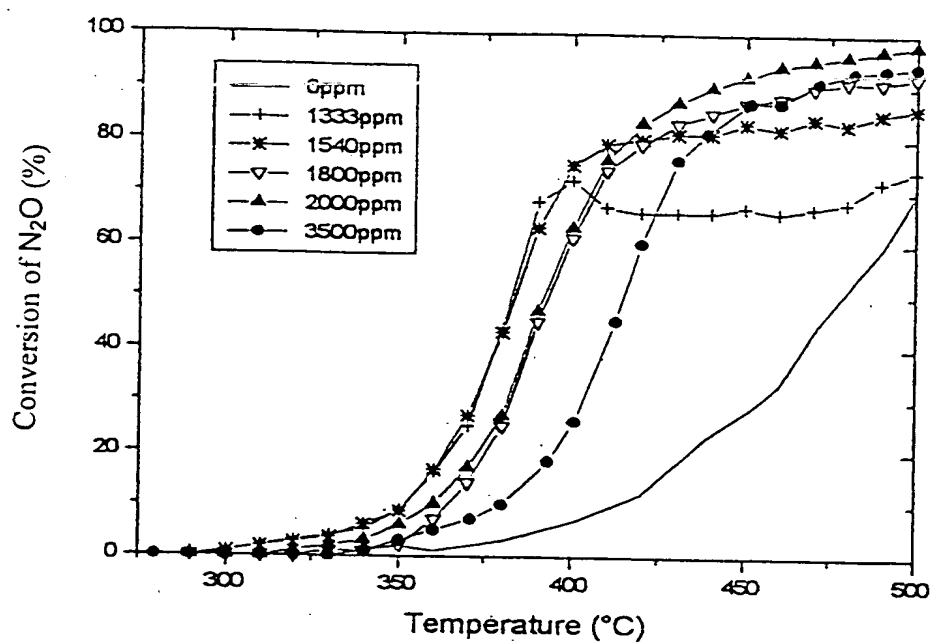


Fig. 2b1: Influence of the NH_3 content on the SCR of $\text{N}_2\text{O} + \text{NO}$ Effect on the NO conversion of N_2O ; VVH = 35000 h^{-1} ; 3% O_2 , 2000 ppm N_2O , 500 ppm NO, x ppm

Catalyst: Fe(49) BEA_e; temperature increasing ($5^\circ\text{C}/\text{min}$)

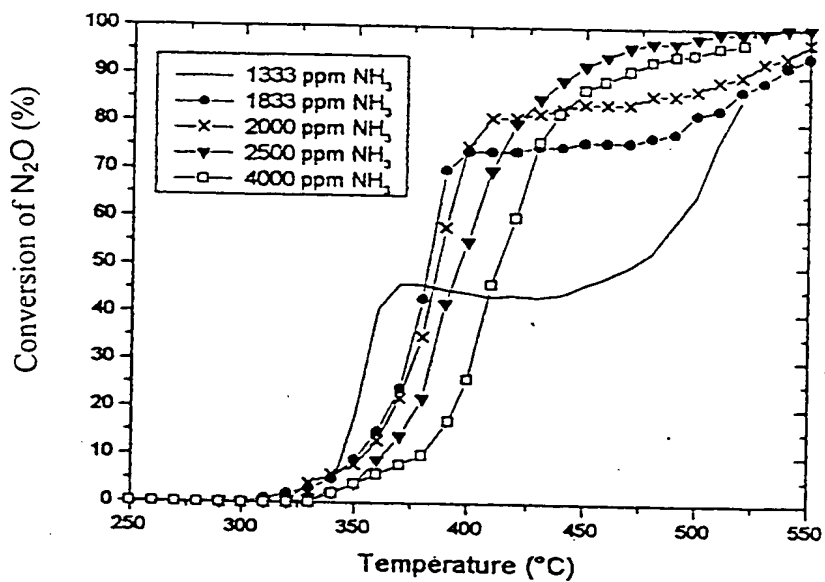


Fig. 2b2: Influence of the NH_3 content on the SCR of $\text{N}_2\text{O} + \text{NO}$: Effect on NO conversion

VVH = 35000 h^{-1} ; 3% O_2 , 2000 ppm N_2O , 500 ppm NO, x ppm NH_3 , He

Catalyst: Fe (49) BEA_6 ; temperature increasing ($5^\circ\text{C}/\text{min}$)

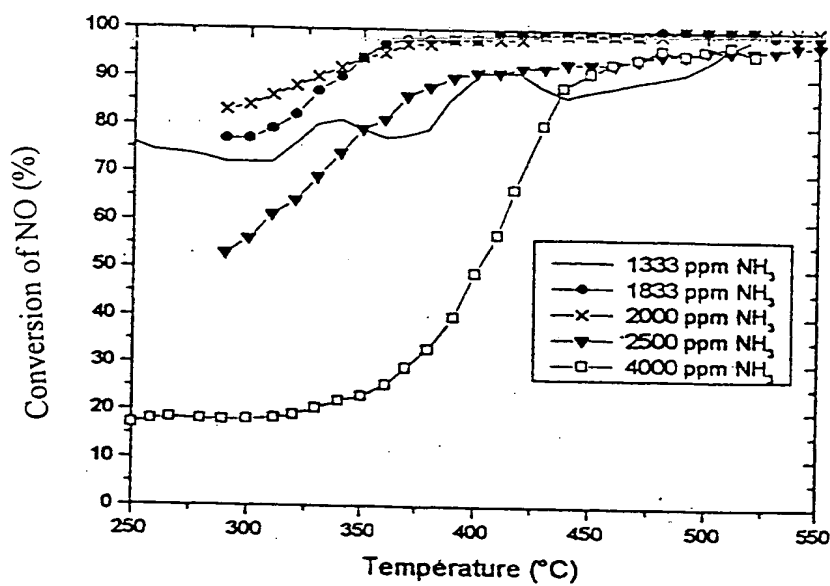


Fig. 3a: SCR of N_2O by NH_3 (2000 ppm/2000 ppm) in the presence of 3% O_2
VVH = 35000 h^{-1} ; Fe, H-BEA catalyst at different iron exchange rates

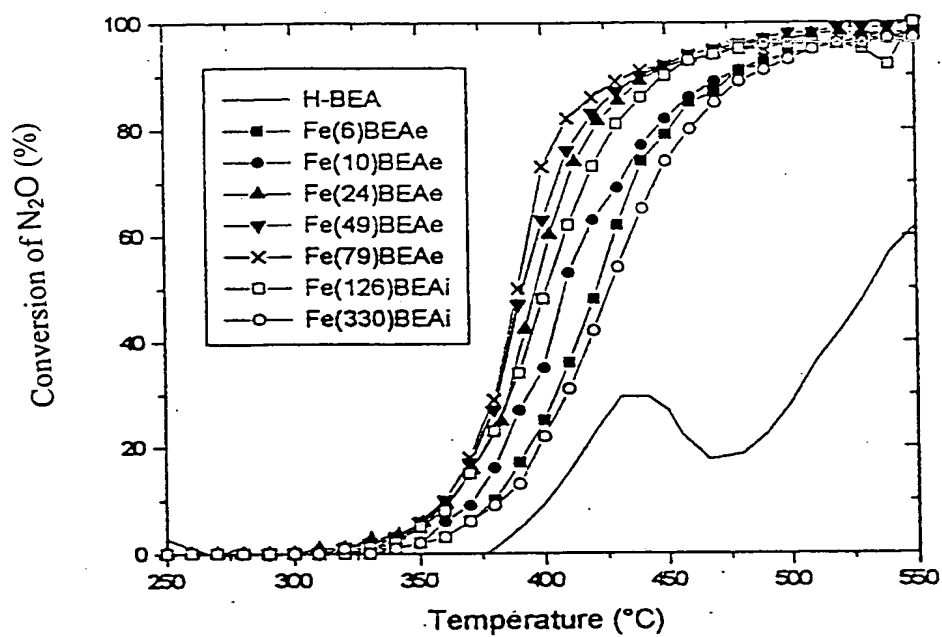


Fig. 3b: Influence of the iron content on the catalytic elimination of NO by NH₃
VVH = 10000 h⁻¹, 3% O₂, 2000 ppm NO, 2000 ppm NH₃, He; descending temperature
stage (1 hour every 10°C); catalyst: FeBEA at different and exchange rates

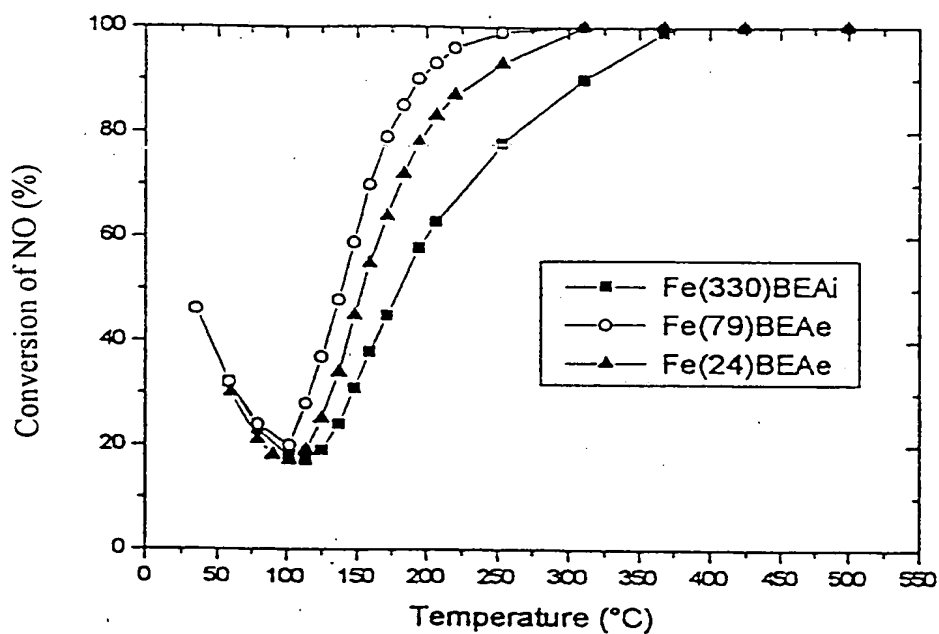


Fig. 3c: Simultaneous elimination of NO and N₂O on FeBEA
VVH = 10000 h⁻¹, 3% O₂, 13500 ppm H₂O, 1500 ppm NO, 1000 ppm N₂O, 2500 ppm
NH₃, 1 hour stage every 10°C

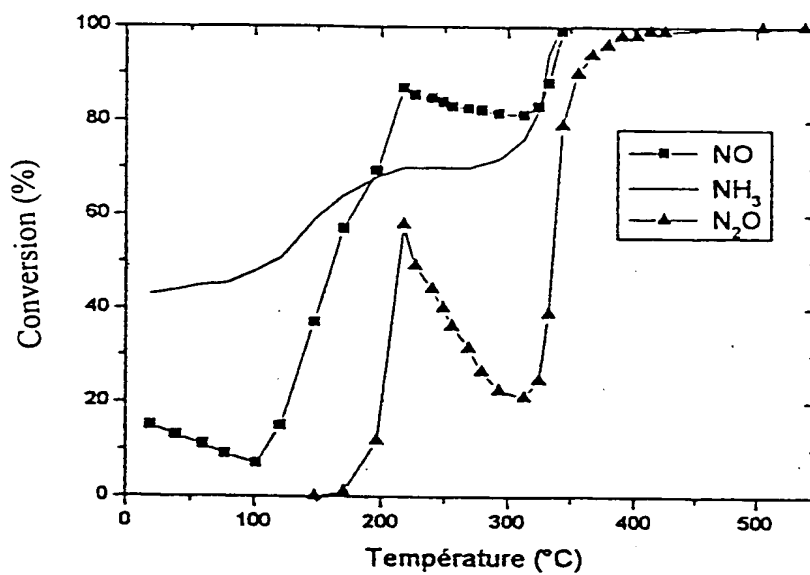


Fig. 4: Influence of the preparation method on SCR of $\text{N}_2\text{O} + \text{NO}$
 $\text{VVH} = 35000 \text{ h}^{-1}$, 3% O_2 , 2000 pm N_2O , 500 ppm NO , 1333 ppm NH_3 ; stage $1\text{h}/10^\circ\text{C}$
 Catalyst: Fe(49) BEA_e; prepared by exchange and Fe(51) BEA_i; prepared by impregnation

